

Name:	 UPES <small>UNIVERSITY WITH A PURPOSE</small>
Enrolment No:	

UNIVERSITY OF PETROLEUM AND ENERGY STUDIES

End Semester Examination, May 2019

Course: Mass Transfer Equipment Design and Separation Processes

Semester: II

Program: M.Tech. Chem Engg (with spl in PDE)

Time: 03 hrs

Course Code: CHPD 7010

Max. Marks: 100

No of pages: 02

Instructions: Assume suitable data, if necessary.

SECTION A

S. No.	Answer any 5 questions. Each carries 12 marks. [12X5=60 Marks]	Marks	CO
Q 1	Describe with flow diagram, Atmospheric Distillation Unit (ADU) of the refinery.	12	CO1
Q.2	Elaborate on 'Equilibrium Solubility of Gases in Liquids'.	12	CO2
Q.3	Discuss 'Choice of Solvent for Liquid-Liquid Extraction.	12	CO3
Q.4	Explain the types of adsorption in detail.	12	CO4
Q.5	Describe with neat sketch, simulation of moving beds for adsorption.	12	CO4
Q.6	Define and explain osmosis and reverse osmosis. Enlist the applications of reverse osmosis along with advantages.	12	CO5

SECTION B

S. No.	Answer both the questions. [35+5 = 40 Marks]																																																																				
Q.7	<p>100 kg of a solution of acetic acid(C) and water (A) containing 30 wt% acid is to be extracted with fresh isopropyl ether (B) at 20°C, in a three stage cross-current liquid extraction. The quantity of solvent to be used in each stage is same i.e. 40 kg. Determine the quantities and compositions of the various streams. How much solvent would be required, in order to achieve same final raffinate concentration, in a single stage cross-current liquid extraction? The equilibrium tie line data at 20°C are as follows:</p> <table border="1" data-bbox="228 558 1230 1073"> <thead> <tr> <th colspan="3" data-bbox="228 558 743 625">Water layer</th> <th colspan="3" data-bbox="743 558 1230 625">Isopropyl ether layer</th> </tr> <tr> <th data-bbox="228 642 440 716">Wt % acetic acid, 100x</th> <th data-bbox="440 642 597 716">Water</th> <th data-bbox="597 642 743 716">Isopropyl ether</th> <th data-bbox="743 642 954 716">Acetic acid, 100y*</th> <th data-bbox="954 642 1084 716">Water</th> <th data-bbox="1084 642 1230 716">Isopropyl ether</th> </tr> </thead> <tbody> <tr><td>0.69</td><td>98.1</td><td>1.2</td><td>0.18</td><td>0.5</td><td>99.3</td></tr> <tr><td>1.41</td><td>97.1</td><td>1.5</td><td>0.37</td><td>0.7</td><td>98.9</td></tr> <tr><td>2.89</td><td>95.5</td><td>1.6</td><td>0.79</td><td>0.8</td><td>98.4</td></tr> <tr><td>6.42</td><td>91.7</td><td>1.9</td><td>1.93</td><td>1.0</td><td>97.1</td></tr> <tr><td>13.30</td><td>84.4</td><td>2.3</td><td>4.82</td><td>1.9</td><td>93.3</td></tr> <tr><td>25.50</td><td>71.1</td><td>3.4</td><td>11.40</td><td>3.9</td><td>84.7</td></tr> <tr><td>36.70</td><td>58.9</td><td>4.4</td><td>21.60</td><td>6.9</td><td>71.5</td></tr> <tr><td>44.30</td><td>45.1</td><td>10.6</td><td>31.10</td><td>10.8</td><td>58.1</td></tr> <tr><td>46.40</td><td>37.1</td><td>16.5</td><td>36.20</td><td>15.1</td><td>48.7</td></tr> </tbody> </table>	Water layer			Isopropyl ether layer			Wt % acetic acid, 100x	Water	Isopropyl ether	Acetic acid, 100y*	Water	Isopropyl ether	0.69	98.1	1.2	0.18	0.5	99.3	1.41	97.1	1.5	0.37	0.7	98.9	2.89	95.5	1.6	0.79	0.8	98.4	6.42	91.7	1.9	1.93	1.0	97.1	13.30	84.4	2.3	4.82	1.9	93.3	25.50	71.1	3.4	11.40	3.9	84.7	36.70	58.9	4.4	21.60	6.9	71.5	44.30	45.1	10.6	31.10	10.8	58.1	46.40	37.1	16.5	36.20	15.1	48.7	35	CO3
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Q.8	<p>An aqueous solution is colored by small amounts of an impurity. It is desired to reduce the color by adsorption. Initial concentration of color is 9.6 units of color / kg solution. It is desired to reduce the color by 90% of its original value. Determine the quantity of fresh carbon required per thousand kg of solution for a single stage operation. Assume equilibrium condition. Equilibrium data at constant temperature:</p> <table border="1" data-bbox="201 1444 1276 1591"> <thead> <tr> <th data-bbox="201 1444 493 1497">kg carbon/kg soln</th> <th data-bbox="493 1444 597 1497">0</th> <th data-bbox="597 1444 743 1497">0.001</th> <th data-bbox="743 1444 889 1497">0.004</th> <th data-bbox="889 1444 1036 1497">0.008</th> <th data-bbox="1036 1444 1182 1497">0.02</th> <th data-bbox="1182 1444 1276 1497">0.04</th> </tr> </thead> <tbody> <tr> <td data-bbox="201 1497 493 1591">Equilibrium color units of color/kg solution</td> <td data-bbox="493 1497 597 1591">9.6</td> <td data-bbox="597 1497 743 1591">8.6</td> <td data-bbox="743 1497 889 1591">6.3</td> <td data-bbox="889 1497 1036 1591">4.3</td> <td data-bbox="1036 1497 1182 1591">1.7</td> <td data-bbox="1182 1497 1276 1591">0.7</td> </tr> </tbody> </table>	kg carbon/kg soln	0	0.001	0.004	0.008	0.02	0.04	Equilibrium color units of color/kg solution	9.6	8.6	6.3	4.3	1.7	0.7	05	CO4																																																				
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