



**UNIVERSITY OF PETROLEUM AND ENERGY STUDIES**

End Semester Examination, December 2021

Course: Chemical Reaction Engineering I

Program: B.Tech (CE+RP)

Course Code: CHCE3004

Semester : V

Duration : 03 hrs.

Max. Marks: 100

**Instructions: (i) In case of data missing make necessary assumptions.**

<b>SECTION A</b>			
<b>(Scan and upload)</b>		<b>(5Qx 4M = 20 Marks)</b>	
<b>Q 1</b>	Enumerate the ways of defining the rate equation.	4	<b>CO1</b>
<b>Q 2</b>	For non-elementary reactions, there is a difference between order and stoichiometric coefficients. Justify the statement.	4	<b>CO1</b>
<b>Q 3</b>	Write the advantages and disadvantages of CSTR.	4	<b>CO3</b>
<b>Q 4</b>	Define $\xi_A$ , Consider a gaseous feed at $T_o = 1000K$ , $P_o = 5$ atm, $C_{A_o} = 100$ moles/lit, $C_{B_o} = 200$ moles/lit enters in a flow reactor in which $A + B \longrightarrow 5C$ occurs. Find $\xi_A$ .	4	<b>CO2</b>
<b>Q 5</b>	What is a semi batch reactor? What are the advantages of this reactor?	4	<b>CO4</b>
<b>SECTION B</b>			
<b>(Scan and upload)</b>		<b>(4Qx10M = 40 Marks)</b>	
<b>Q 1</b>	Discuss the theory of maximization of rectangles for finding optimum sizes of two mixed reactors in series.	10	<b>CO5</b>
<b>Q 2</b>	For $A \longrightarrow R \longrightarrow S$ derive an expression for $C_{R_{max}}$ by considering unimolecular type first order reaction. Assume $K_1$ and $K_2$ as rate constants.	10	<b>CO2</b>
<b>Q 3</b>	A homogeneous liquid phase reaction with the stoichiometry and the kinetics $A \longrightarrow S$ , $-r_A = kC_A^2$ , takes place with 50% conversion in a mixed flow reactor. If this MFR is replaced by a PFR of the same size, find the conversion in PFR. All other conditions are remaining unchanged.	10	<b>CO4</b>
<b>Q 4</b>	It is required to produce 9.5 kg/s of ethylene by cracking a feed stream of pure ethane in a plug flow reactor operated at 1100 K and 6 atm. The cracking reaction is first order with $K = 3.07 / s$ . at 1100 K. $C_2H_6 \longrightarrow C_2H_4 + H_2$ Find the volume of reactor to achieve 80 % conversion of ethane.	10	<b>CO3</b>
<b>SECTION-C</b>			
<b>(Scan and upload)</b>		<b>(2Qx 20M= 40 Marks)</b>	
<b>Q 1</b>	Substance A in liquid phase produces R and S by the following reactions $A \longrightarrow R$ $A \longrightarrow S$ With $r_R = K_1 C_A^2$ and $r_S = K_2 C_A$ . the feed ( $C_{A_o} = 1.0$ mol/lit, $C_{R_o} = 0$ , $C_{S_o} = 0.30$ mol/lit) enters two mixed flow reactors in series ( $\tau_1 = 2.5$ min, $\tau_2 = 2.5$ min) knowing the composition in the first order ( $C_{A_1} = 0.4$ mol/lit, $C_{R_1} = 0.2$ mol/lit, $C_{S_1} = 0.70$ mol/lit), find the composition leaving the second reactor.	20	<b>CO5</b>
<b>Q 2</b>	The elementary gas phase reaction $A_3 \longrightarrow 3A$ is carried out in a plug flow reactor. The rate constant at 50°C is $10^{-4} \text{ min}^{-1}$ and the activation energy is 85 kJ/mol. Pure $A_3$ enters the reactor at 10 atm and 127°C and a molar flow rate of 2.5 mol/min. Calculate the reactor volume and the space time required to achieve 90% conversion of $A_3$ . Assume applicability of Arrhenius law.	20	<b>CO4</b>