

<b>Name:</b>	 <b>UPES</b> <small>UNIVERSITY OF TOMORROW</small>
<b>Enrolment No:</b>	

**UNIVERSITY OF PETROLEUM AND ENERGY STUDIES**  
**End Term Examination, December 2022**

<b>Programme Name: B.Tech APE Gas</b>	<b>Semester : V</b>
<b>Course Name : Gasification and Gas to Liquid Technology</b>	<b>Time : 3 hr</b>
<b>Course Code : CHGS3008P</b>	<b>Max. Marks: 100</b>
<b>Nos. of page(s) : 2</b>	

**Instructions: Answer the questions in sequence.**

**SECTION A (Attempt all questions)**

S. No.		Marks	CO																		
Q1.	a) Define biomass, sources of biomass and its utilization. b) Illustrate the challenges in the use of biomass.	<b>(6+6)</b> <b>12M</b>	<b>CO1</b>																		
Q2.	<p>Wood pellets are gasified in an open core throatless gasifier. The initial design conditions are given in the below table.</p> <table border="1" style="width: 100%; margin-bottom: 10px;"> <tr><td>Type of gasifier</td><td>Downdraft Throatless</td></tr> <tr><td>Type of fuel</td><td>Wood pellets</td></tr> <tr><td>Calorific value of fuel</td><td>14 MJ/kg</td></tr> <tr><td>Density of fuel</td><td>375 kg/m<sup>3</sup></td></tr> <tr><td>Gasification efficiency</td><td>60%</td></tr> <tr><td>Specific Gasification Rate</td><td>120 kg/m<sup>2</sup> h</td></tr> <tr><td>Equivalence Ratio</td><td>0.25</td></tr> <tr><td>Stoichiometric Air to Fuel Ratio</td><td>6.5 kg of air/Kg of wood</td></tr> <tr><td>Net Energy</td><td>6 kW</td></tr> </table> <p>Calculate a) Fuel Consumption rate b) Cross Sectional area of the reactor c) Diameter of the reactor d) Height of reactor e) Air flow rate f) Superficial air velocity</p>	Type of gasifier	Downdraft Throatless	Type of fuel	Wood pellets	Calorific value of fuel	14 MJ/kg	Density of fuel	375 kg/m <sup>3</sup>	Gasification efficiency	60%	Specific Gasification Rate	120 kg/m <sup>2</sup> h	Equivalence Ratio	0.25	Stoichiometric Air to Fuel Ratio	6.5 kg of air/Kg of wood	Net Energy	6 kW	<b>12M</b>	<b>CO2</b>
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Q3.	Explain the phenomenon of Fluidization and explain the working of a circulating fluidized bed gasifier with a neat diagram.	<b>12M</b>	<b>CO2</b>																		
Q4.	Syngas produced from coal gasification needs to be cleaned and conditioned for downstream processing. Illustrate.	<b>12M</b>	<b>CO3</b>																		

Q5.	Compare the different reactor configurations for Fischer-Tropsch Synthesis to produce liquid products from syngas.	12M	CO4
<b>SECTION B</b> <b>(Q6 is Compulsory &amp; Answer any one from Q7)</b>			
Q6.	Coal has the following composition on mass basis %C-73.2, H-5.2, O-13.6, N-1.3, S-1.7, Moisture-5. If the above material is gasified in a downdraft gasifier what will be the composition of the gas produced when coal to oxygen ratio is 0.5 mass of coal/mass of oxygen and steam to coal ratio is 0.5 mass/mass. Assume CO to H <sub>2</sub> is 2:1 vol/vol. Ignore the presence of impurities. Find the molecular weight of coal and composition of the product gas and CO and Hydrogen yield.	20M	CO3
Q7.	a) Calculate the mass of methanol (in lb) that can be produced from 4 Bcf of natural gas. Assume that it is all methane. How many pounds of oxygen would be required? b) With a basic flow chart outline the process of indirect conversion of natural gas to liquids through syngas and Fischer-Tropsch synthesis.	(5+15) 20M	CO4
<b>(Or)</b>			
	a) Discuss the Biomass to Liquids -Fischer -Tropsch final fuel products in detail. b) Summarize the role of catalysts in the hydrogenation of carbon monoxide to higher hydrocarbons.	(10+10) 20M	CO4