


Name:										
Enrolment No:										
UNIVERSITY OF PETROLEUM AND ENERGY STUDIES End Semester Examination, May 2022										
Course: Process Modelling and Simulation Program: M. Tech Chemical Engineering Course Code: CHPD7009					Semester : II Time : 03 hrs. Max. Marks: 100					
Instructions:										
SECTION A (5Qx4M=20Marks)										
S. No.									Marks	CO
Q 1	State the importance of assumptions in model development.								04	CO1
Q 2	Discuss the sequential modular approach of process simulation								04	CO1
Q 3	Explain about the mathematical consistency of a process model.								04	CO1
Q 4	Distinguish between steady state model and dynamic model.								04	CO2
Q 5	Discuss about distributed parameter system.								04	CO2
SECTION B (4Qx10M= 40 Marks)										
Q 6	Regress the data given in Table 1 to the form $y = a(1 + x^2)^n$ using the method of least squares. Table 1: Data on x and y								10	CO2
	x	0.0	0.5	1.0	1.5	2.0	2.5	3.0		
	y	1.00	0.89	0.71	0.55	0.44	0.37	0.31	0.27	0.24
Q 7	Develop the mass balance equations for a double effect evaporator system.								10	CO3
Q 8	Discuss about the formulation of Kb method used to compute new temperature profile in multicomponent distillation column. <p style="text-align: center;"><i>OR</i></p> Write down a set of model equations for multicomponent distillation column with multiple stages.								10	CO4
Q 9	State the application of orthogonal collocation method in chemical engineering system.								10	CO5
SECTION-C (2Qx20M=40 Marks)										

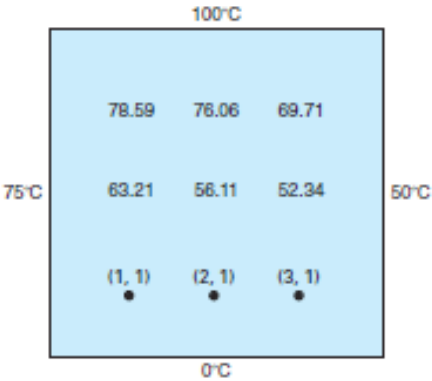
<p>Q 10</p>	<p>Develop a two dimensional pseudo heterogeneous model of fixed bed reactor with suitable boundary conditions. State the assumptions clearly.</p> <p style="text-align: center;"><i>OR</i></p> <p>Consider a special (diameter = 10 cm) ball made of steel ($k = 40 \text{ W/mK}$, $\rho = 8000 \text{ kg/m}^3$, $C_p = 400 \text{ J/kgk}$). The initial temperature of the ball is 300 K. It is immersed in a large oil tank at 400 K. The convective heat transfer coefficient, h at the sphere surface is $3000 \text{ W/m}^2\text{k}$. Assume that there is no radial temperature gradient inside the ball. Use the RK-4 numerical technique to solve the governing first order energy balance equation for predicting the temperature of the sphere at $t = 1 \text{ min}$ after it was immersed in the oil tank. Use $\Delta t = 30 \text{ s}$. Calculate the rate of temperature-decrease at $t = 0, 0.5$ and 1.0 min.</p>	<p>20</p>	<p>CO4</p>
<p>Q 11</p>	<p>Apply the central difference method to Laplace equation given below to find out $T(1,1)$, $T(2,1)$ and $T(3,1)$ where $\Delta x = \Delta y$.</p> $\frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} = 0$ <div style="text-align: center;">  </div>	<p>20</p>	<p>CO5</p>

Fig. 1 A heated plate