


Name:			
Enrolment No:			
UNIVERSITY OF PETROLEUM AND ENERGY STUDIES End Semester Examination, May 2023			
Programme Name: M Tech (Chemical Engineering)		Semester : II	
Course Name : Advanced Thermodynamics		Time : 03 hrs	
Course Code : CHPD7003		Max. Marks: 100	
Nos. of page(s) : 2			
Instructions: Assume the values of parameters logically where necessary			
SECTION A			
S. No.		Marks	CO
Q 1	Define Work thermodynamically. Provide a short discuss on the different classifications of Work generally encountered in thermodynamic system.	4	CO1
Q 2	Are 1 N and 1 kgf (kg-force) similar quantity? Provide the correct definition for each term.	4	CO1
Q 3	Provide your argument why Gibbs Free Energy is considered as the generating function for various thermodynamic relationships. Explain with example.	4	CO1
Q 4	Discuss concisely the difference between the Clausius-Clapeyron and modified Clausius-Clapeyron equation.	4	CO2
Q 5	Define Corresponding States Principle and draw a representative plot.	4	CO2
SECTION B			
Q 6	Discuss the conditions for test for exactness used in partial differential equation with an example.	10	CO3
Q 7	Apply the 1 st law of thermodynamics to derive the expression for energy and work. Or Derive the expression for vapor/liquid phase equilibrium of a pure component with mass transfer.	10	CO3
Q 8	Air at 1 bar and 25°C enters a compressor at low velocity, discharges at 3 bar, and enters a nozzle in which it expands to a final velocity of 600 m/s at the initial conditions of pressure and temperature. If the work of compression is 240 kJ per kilogram of air, how much heat must be removed during compression?	10	CO4
Q 9	Apply the 1 st law of thermodynamics formulation to derive the Maxwell's relationship dh = Tds + vdP	10	CO4
SECTION C			
Q 10	A liquid-vapor mixture contains n-hexane (component 1) and n-heptane (component 2) at 27°C. Estimate the composition of the liquid and vapor phases as a function of total pressure if the phases behave as ideal solution. Plot the results in P-x-y diagram. P1 and P2 are the vapor pressure of pure n-hexane and pure n-heptane respectively. $\ln P_1 = 18.057 - (3837.4/T)$ $\ln P_2 = 18.217 - (4231.0/T)$ or	20	CO5

	Calculate the internal energy and enthalpy changes resulting if air changes from an initial state of 5°C and 10 bar, where its molar volume is $2.312 \times 10^{-3} \text{ m}^3/\text{mol}$, to a final state of 60°C and 1 bar. Assume also that air remains a gas for which PV/T is constant and that $CV = 20.785$ and $CP = 29.100 \text{ J/mol K}$																							
Q 11	<p>Acetic acid is esterified in the liquid phase with ethanol at 100°C and atmospheric pressure to produce ethyl acetate and water according to the reaction: $\text{CH}_3\text{COOH (l)} + \text{C}_2\text{H}_5\text{OH (l)} \rightarrow \text{CH}_3\text{COOC}_2\text{H}_5\text{(l)} + \text{H}_2\text{O(l)}$</p> <p>If initially there is one mole each of acetic acid and ethanol, estimate the mole fraction of ethyl acetate in the reacting mixture at equilibrium.</p> <table border="1" data-bbox="224 598 1292 892"> <thead> <tr> <th></th> <th>ΔH_{f298}°</th> <th>ΔG_{f298}°</th> </tr> </thead> <tbody> <tr> <td>ethyl acetate (l)</td> <td>- 480,000</td> <td>- 332,200</td> </tr> <tr> <td>acetic acid (l)</td> <td>-484,500</td> <td>-389,900</td> </tr> <tr> <td>Ethanol (l)</td> <td>-277,690</td> <td>-174,780</td> </tr> <tr> <td>Ethanol (g)</td> <td>-235,100</td> <td>-168,490</td> </tr> <tr> <td>Water (g)</td> <td>-241,818</td> <td>-228,572</td> </tr> <tr> <td>Water (l)</td> <td>-285,830</td> <td>-237,129</td> </tr> </tbody> </table>		ΔH_{f298}°	ΔG_{f298}°	ethyl acetate (l)	- 480,000	- 332,200	acetic acid (l)	-484,500	-389,900	Ethanol (l)	-277,690	-174,780	Ethanol (g)	-235,100	-168,490	Water (g)	-241,818	-228,572	Water (l)	-285,830	-237,129	20	CO5
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