


Name:			
Enrolment No:			
UPES End Semester Examination, May 2024			
Programme Name: B. Tech Chemical Engg.		Semester : IV	
Course Name : Chemical Engineering Thermodynamics 2		Time : 3 hrs	
Course Code : CHCE2008		Max. Marks: 100	
Nos. of page(s) : 02			
Instructions: (1) This is an OPEN BOOKS and OPEN NOTES Examination. (2) Assume the appropriate value of missing data, if any. (3) The thermodynamic terms have their usual meanings			
(Answer all questions)			
S. No.		Marks	CO
1.	A binary mixture of dioxane (1) -steam (2) forms and azeotrope at 345 K during the separation of the mixture by distillation. The activity coefficient of both the components can be calculated as $\overline{G}_1^E = Ax_2^2 = RT \ln \gamma_1$ $\overline{G}_2^E = Ax_1^2 = RT \ln \gamma_2$ The saturation vapor pressures are given as, $P_1^{sat} = 15.6$ kPa and $P_2^{sat} = 12.4$ kPa . Calculate the value of A, if azeotropic composition is $x_1 = 0.51$.	20	CO3
2.	Three students from the Department of Chemical Engineering at UPES Dehradun working in the research lab conducted experiments on a binary hexane (1)-water (2) system to gather data on activity coefficients. After conducting multiple experiments under consistent temperature and pressure conditions, they obtained values for the activity coefficients of hexane (1)-water (2) as follows $\gamma_1 = \exp[x_2^2(2x_1 + 0.5)]$ and $\gamma_2 = \exp[x_1^2(-2x_2 + 1.5)]$. As a chemical engineer, could you evaluate the accuracy of their estimations? Calculate the excess Gibbs free energy of the mixture containing 40 mole % of hexane at 335 K.	20	CO4

3.	<p>What are some of the most challenging aspects of predicting and controlling chemical reaction equilibria in industrial chemical processes? How can thermodynamic modeling and experimental techniques address these challenges? [Hint: I am providing you 2 challenging aspects, multiple reactions and non-ideal behavior. You are expected to provide 2 more challenging aspects and elaborate how can you address them using theoretical knowledge of thermodynamics and experimental techniques.</p>	5+20	CO1, CO4																											
4	<p>The following experimental VLE data at 760 Torr is obtained for hexane (1)-water (2) system. The system follows van Laar model of activity coefficients. From the given data, obtain VLE data (make a table for the following data $t, x_1, y_1, P_1^s, P_2^s, \ln \gamma_1, \ln \gamma_2, P, RTx_1x_2 / G^E$) and plot RTx_1x_2 / G^E vs x_1 and find the van Laar constants A and B from the plot. The following data is available for the system,</p> <table border="1" data-bbox="207 930 592 1144"> <thead> <tr> <th>t(deg C)</th> <th>x_1</th> <th>y_1</th> </tr> </thead> <tbody> <tr> <td>96.9</td> <td>0.015</td> <td>0.133</td> </tr> <tr> <td>68.2</td> <td>0.426</td> <td>0.747</td> </tr> <tr> <td>65.1</td> <td>0.747</td> <td>0.838</td> </tr> <tr> <td>64.5</td> <td>0.914</td> <td>0.921</td> </tr> </tbody> </table> <p>The van Laar Model is given by,</p> $\frac{G^E}{RTx_1x_2} = \frac{A}{\left(\frac{A}{B}\right)^{x_1+x_2}}$ <p>The Antoine constants are given as, $[\log_{10} P = A - \frac{B}{t+C}]$, P is in Torr and t is in deg C]</p> <table border="1" data-bbox="207 1493 885 1617"> <thead> <tr> <th></th> <th>A</th> <th>B</th> <th>C</th> </tr> </thead> <tbody> <tr> <td>Hexane</td> <td>8.081</td> <td>1582.3</td> <td>239.726</td> </tr> <tr> <td>Water</td> <td>7.2817</td> <td>1446.9</td> <td>227.6</td> </tr> </tbody> </table>	t(deg C)	x_1	y_1	96.9	0.015	0.133	68.2	0.426	0.747	65.1	0.747	0.838	64.5	0.914	0.921		A	B	C	Hexane	8.081	1582.3	239.726	Water	7.2817	1446.9	227.6	15+20	CO2, CO4
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