

Name:

Enrolment No:



UPES, Dehradun

End Semester Examination, April-May 2024

Program Name : B. Tech. (CE&RP)

Semester : VI

Course Name : Process Dynamics Instrumentation & control

Time : 3 hours

Course Code : CHCE3007

Max. Marks : 100

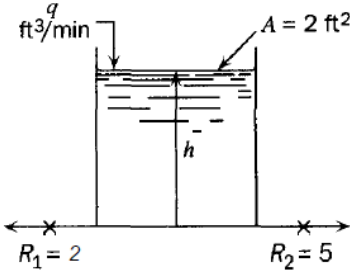
Nos. of page(s) : 02

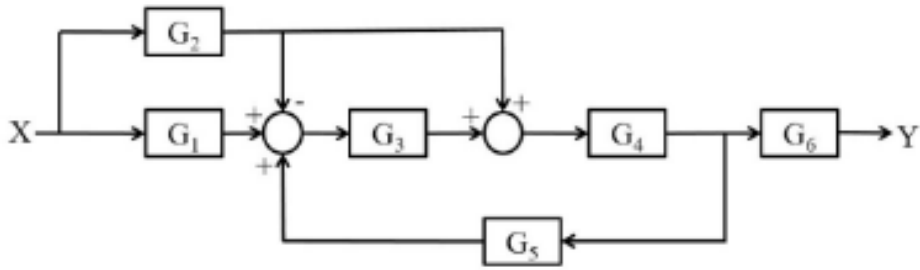
Instructions : Assume any missing data. Draw the diagrams, wherever necessary. Write roll number and name on any additional sheet that you use.

SECTION A
(5X4=20 marks)

S. No.		Marks	CO
1	Identify the terms used in underdamped second order system?	4	CO1
2	List the assumptions used in the mercury in glass bulb thermometer model.	4	CO1
3	Describe damping?	4	CO2
4	Summarize Routh stability criterion.	4	CO2
5	Demonstrate the way how root locus is plotted	4	CO3

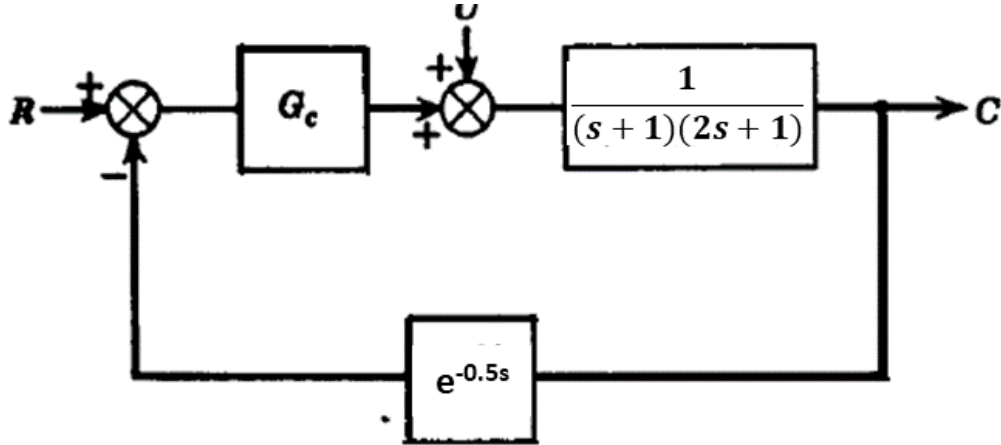
SECTION B
(4X10=40 marks)

6	Outline the following differential equations using Laplace Transforms. a) $\frac{dx}{dt} - x = e^{3t}$ $x(0) = 2$ b) $\frac{d^2x}{dt^2} - \frac{dx}{dt} + 2x = e^{3t}$ $x(0) = 1$ and $x'(0) = 0$	10	CO1
7	There are N storage tank of volume V Arranged so that when water is fed into the first tank into the second tank and so on. Each tank initially contains component A at some concentration C_0 and is equipped with a perfect stirrer. A time zero, a stream of zero concentration is fed into the first tank at volumetric rate q . Predict the resulting concentration in each tank as a function of time.	10	CO2
8	 <i>Demonstrate</i> expression for $H(s)/Q(s)$. Substitute the appropriate values in the transfer function and report.	10	CO3
9	<i>Appraise</i> the reduction of given block diagram and find Y/X	10	CO4



SECTION C
(2 X 20=40 marks)

Without plotting the bode diagram, evaluate the tuning parameters for PID controller using Ziegler and Nichols control settings.



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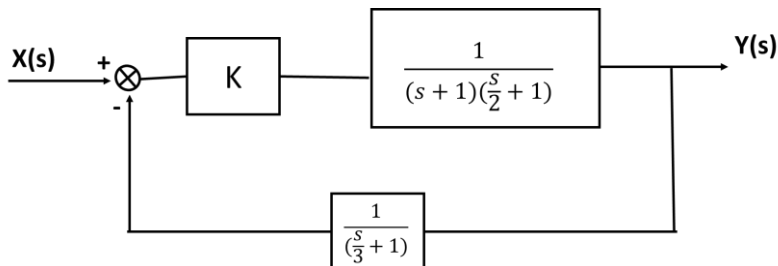
CO5

OR

Plot the root locus for the open loop transfer function

$$1 + \frac{K(0.5s + 1)}{s(s + 1)(2s + 1)}$$

- a) In the control system shown above, *interpret* the value of K for which the system is stable. The controller is replaced by a PI controller with transfer function $K \left(1 + \frac{1}{\tau_I s} \right)$. If $K = 10$, determine the range of τ_I for which the system is stable.



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10

CO4

- b) Three identical tanks are operated in series in a non-interacting fashion. For each tank $R=1$, $\tau = 1$. If the deviation in flow rate to the first tank in an impulse function of magnitude 2, Predict an expression for $H(s)$ where H is the deviation in level in the third tank and obtain the deviation value at time $t=1.5$.

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